

REMARKS

The claims have been amended to delete all multiple dependencies.

Attached are the search reports of the corresponding PCT and French applications, together with copies of the references cited therein, which are listed on the attached Form PTO-1449.

Respectfully submitted,

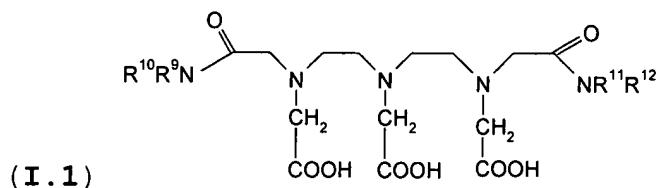


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APPENDIX

3. (Amended) Process according to claim 1 [or 2], characterized in that the molecular weight of the ligands (I) used is greater than the cut-off threshold of the nanofiltration membrane.

4. (Amended) Process according to claim 1 [or claim 2], characterized in that a ligand of formula (I.1) is used:



in which R^9 , R^{10} , R^{11} and R^{12} are identical to or different from one another and are each a hydrophilic monovalent radical having the same definition as that given for R^9 and R^{10} in claim 1, ethanoyl, methoxyethyl and sorbitoyl radicals being more especially preferred.

5. (Amended) Process according to [any one of claims 1 to 4] claim 1, characterized in that several metal species belonging to the lanthanide and/or actinide family are separated, said separation being effected by successive complexations of the ions of each of these species to be

separated, the appropriate selective ligand being chosen for each species (step 1) and a nanofiltration (step 2) and a decomplexation/collection (step 3) being carried out after each complexation.

6. (Amended) Process according to [any one of claims 1 to 5] claim 1, characterized in that the nanofiltration membrane used is made of at least one material selected from the group of polymers [comprising] consisting of:

polyaramides, sulfonated polysulfones,
polybenzimidazolones, grafted or non-grafted polyvinylidene fluorides, polyamides, cellulose esters, cellulose ethers, perfluorinated ionomers, associations of these polymers, and copolymers obtained from monomers of at least two of these polymers.

7. (Amended) Process according to [any one of claims 1 to 6] claim 1, characterized in that the selected membrane has a cut-off threshold, expressed in g/mol, which is defined as follows:

	100 - 5000
preferably	200 - 2000
and even more preferably	500 - 1500

8. (Amended) Process according to [any one of claims 1 to 7] claim 1, characterized in that the pH of the medium, preferably the aqueous solution, constituting the

complexation/ separation medium is fixed at between 1 and 6.

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